

# Modeling and Optimization of Carbon Dioxide Removal in Packed Bed Column Reactor

K. Thirugnanasambandham

State University of Maringá, Department of Chemical Engineering, Av. Colombo, Maringá-PR, Brazil  
E-Mail: thirusambath5@gmail.com

(Received 4 June 2019; Accepted 24 July 2019; Available online 1 August 2019)

**Abstract** - Global warming due to greenhouse gases has become a serious global issue. Extensive efforts are being made to fighting this phenomenon through carbon capture as carbon dioxide (CO<sub>2</sub>) is its major contributor. This study focused on CO<sub>2</sub> capture in packed bed column reactor using Poly-(D) glucosamine under the various process parameters such as temperature, feed flow rate and mass of the adsorbent. Statistical design of experiments was carried out in order to analysis the effect process parameters on the capacity of CO<sub>2</sub> capture in packed bed column. The obtained results show that feed flow rate has the significant affect compared to others. The maximum of 956 mg of CO<sub>2</sub> is captured under the following operating conditions; temperature of 40°C, feed flow rate of 30 ml/min and 0.25 g of the Poly-(D) glucosamine. The ability of Poly-(D) glucosamine to capture the CO<sub>2</sub> in packed bed column is confirmed.

**Keywords:** CO<sub>2</sub> Capture, Packed Bed Column, Poly-(D) Glucosamine, Adsorption, Optimization

## I. INTRODUCTION

Nowadays, fossil fuels are the key conventional energy source and consumption of them will increase constantly, every day [1]. The combustion of very huge amount of fossil fuels releases, carbon dioxide and other greenhouse gases that have a significant impact on global warming and climate change. The global warming and greenhouse effect have become serious global environmental issues [2]. The content of carbon dioxide in the atmosphere has increased from  $2.84 \times 10^{-4}$  before the industrial revolution to  $3.56 \times 10^{-4}$ . Hence, the stability, safety and environment acceptability of CO<sub>2</sub> capture methods have been paid worldwide notice. Therefore, there is critical need to develop a technology, which reduces the carbon dioxide in atmosphere [3].

The technologies include the chemical absorption and adsorption methods, membrane separation and chemical looping combustion, underground storage technology, terrestrial vegetation and marine microalgae fixation were used for CO<sub>2</sub> capture. Among these technologies, adsorption is the most favorable technique because of its advantages such as high adsorption capacity, low cost and easy to operate [4]. Moreover, the key desired characteristics of the adsorbent in adsorption is high density (it allows operation at higher velocity, so smaller adsorber vessels are needed for carrying out preferred level of separation), a wide particle size allocation and high porosity (reduced mass transfer resistances and resulting in enhanced dynamic

adsorption capacity. Packed beds reactors are mainly used for CO<sub>2</sub> capture using various adsorbents [5]. The advantage of using a packed bed reactor is the higher conversion per weight of catalyst than other catalytic reactors [6]. The conversion is based on the amount of the solid catalyst rather than the volume of the reactor. Many researchers have reported the impact of parameters (temperature, feed flow rate and mass of the adsorbent) on the performance of packed beds, with different adsorbents and columns. Moreover, optimization of these parameters will improve the adsorption performance [7-9].

Best of our knowledge, none of studies were reported for the CO<sub>2</sub> capture in packed bed column via statistical methods. Response surface methodology (RSM) coupled with Box-Behnken design (BBD) is a statistical method which used to analyze the influence of effect process parameters in various process [10]. Hence, in this study an attempt has been made to study the individual and interactive effect of process parameters such as temperature, feed flow rate and mass of the adsorbent on CO<sub>2</sub> capture in packed bed column. Also the response surface methodology coupled with numerical optimization was applied to model and optimize the CO<sub>2</sub> capture process in packed bed column. It is believed that, the results obtained from this study will be useful understand the relationship between the process parameters and CO<sub>2</sub> capture, mathematically.

## II. MATERIALS AND METHODS

### A. Chemicals and Experimental Setup

The entire chemical used in this study is analytical grade and purchased from local suppliers. The experimental set up used in this study was reported in elsewhere (Muofhe *et al.*, 2017) with slight modifications. The performance evaluation of Poly-(D) glucosamine was determined using a gas mixture containing CO<sub>2</sub> (15%) and N<sub>2</sub> (85%).

### B. Modeling

Response surface methodology (RSM) coupled with Box-Behnken design (BBD) was used to analyze the influence of effect process parameters on CO<sub>2</sub> capture in packed bed column. Experimental runs were established based on a BBD and the complete design consists of 17 experiments were designed and the obtained data was analyzed by

multiple regression analysis [11]. Then, the individual and interactive effects of process variables on CO<sub>2</sub> capture in packed bed column were determined by constructing response surface plots. Finally, optimization of process variables for maximum CO<sub>2</sub> capture was carried out by numerical optimization technique [12]. All the statistical analyses were carried out with Stat ease Design Expert 8.0.7.1.

### III. RESULTS AND DISCUSSION

#### A. Effect of Temperature

Temperature is one of the key process variables for the packed bed column performance on CO<sub>2</sub> capture. To

examine effect of temperature on CO<sub>2</sub> capture experiments were carried out in temperature (25– 75°C) and the results are shown in Fig. 1.

From the observations, it is found that, the CO<sub>2</sub> capture is increased rapidly with increasing the temperature upto 60°C. This phenomenon could be explained by that, the increase in temperature increases the adsorption capacity Poly-(D) glucosamine, which improves the CO<sub>2</sub> capture.

Beyond, temperature of 60°C shows the negligible effect on CO<sub>2</sub> capture. Similar observations were obtained for carbon dioxide adsorption hysteresis in ultramicroporous metal-organic frameworks (MOFs) [13].

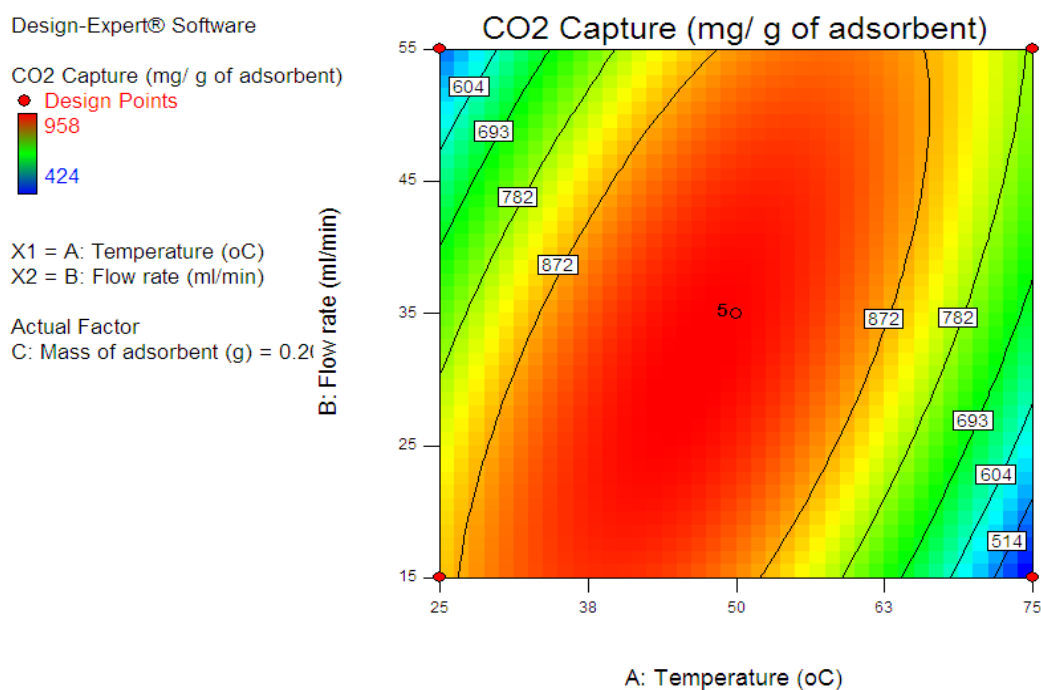


Fig. 1 Response surface plots representing the effect of process variables on CO<sub>2</sub> capture (A and B)

#### B. Effect of Flow Rate

Flow rate is one of the most important parameter that affects the CO<sub>2</sub> capture in packed bed column, significantly. In order to study the effect of flow rate on CO<sub>2</sub> capture in packed bed column, experiments were carried out in various flow rates (15-55 ml/min) and results are depicted in Fig. 2.

From the results, it is found that CO<sub>2</sub> capture in packed bed column is increased with increasing flow rate upto 45 ml/min. This may be due to the fact that more mixture would be spread on the packing surface, and this leads to an increase in the interfacial area per unit volume and hence CO<sub>2</sub> capture in packed bed column is increased. Thereafter, there is a negligible effect on the CO<sub>2</sub> capture. Similar kind of results was obtained for CO<sub>2</sub> adsorption from ambient air using a supported amine based sorbent in a fixed bed reactor [14].

#### C. Effect of Mass of Adsorbent

Mass of the adsorbent used in CO<sub>2</sub> capture in packed bed column significantly affects the process performance. Because the surface of adsorbent is the main factor to adsorption and it is directly proportional to mass. Hence, various adsorbent mass (0.1-0.3 g) are employed in order to determine its effect on CO<sub>2</sub> capture in packed bed column.

From the results (Fig. 3), it was observed that, the maximum CO<sub>2</sub> capture in packed bed column is obtained in 0.25g. This can explain by the fact that, reactive sites are directly proportional to mass. Hence, CO<sub>2</sub> capture is increased with increasing mass of adsorbent. The trend obtained this study is close agreement with CO<sub>2</sub> adsorbent developed with high adsorption properties in a coal mine refuge chamber [15].

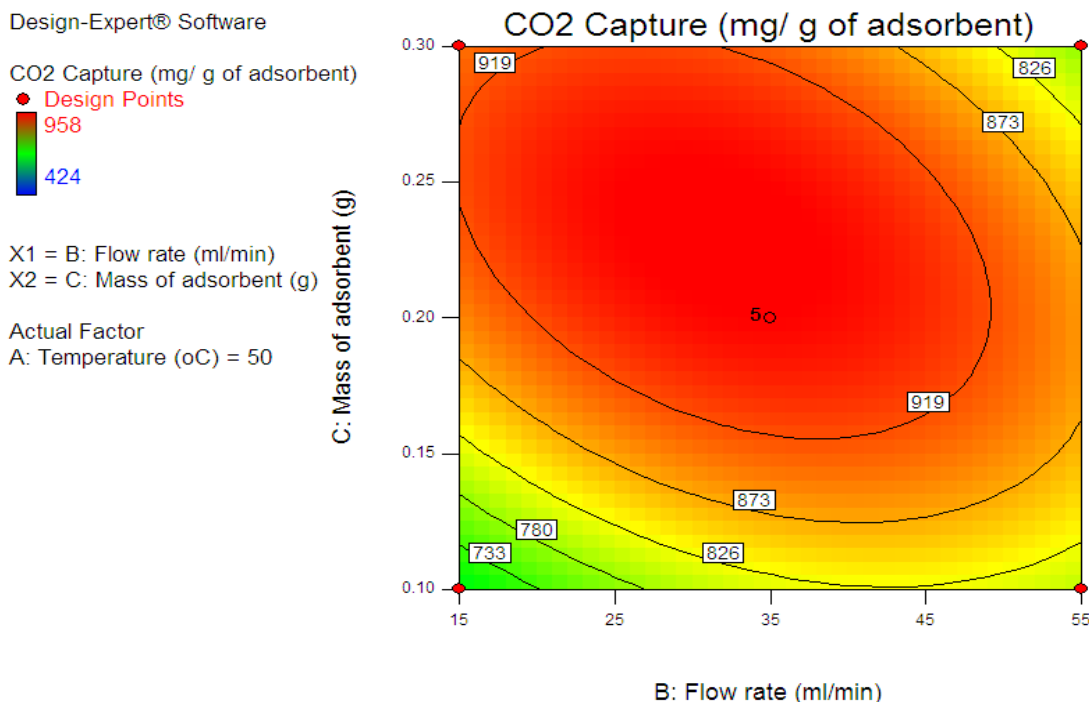


Fig. 2 Response surface plots representing the effect of process variables on CO<sub>2</sub> capture (A and B)

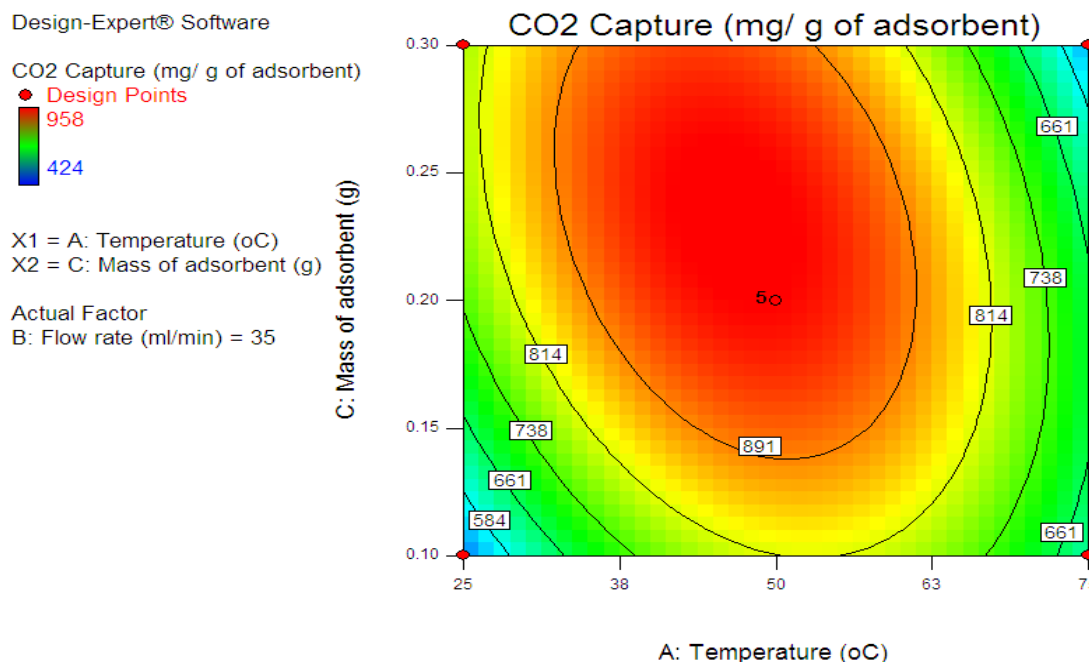


Fig. 3 Response surface plots representing the effect of process variables on CO<sub>2</sub> capture (A and C)

*D. Statistical Analysis*

CO<sub>2</sub> capture in packed bed column is examined by statistical method using RSM. Three factors three levels Box-Behnken response surface design (BBD) is used in order to estimate and optimize the effect of process variables in packed bed column. A total number of 17 experiments were carried out (Table I) and the response is CO<sub>2</sub> Capture (R<sub>1</sub>: mg/g of adsorbent). The response values obtained in BBD are analyzed by multi regression analysis

(Table II) in order to select the effective model among various models such as linear, interactive (2FI), quadratic and cubic to explain the CO<sub>2</sub> Capture. From the results, it is found that second order polynomial model is found to be best fit with F value and lower p value. Therefore the second order polynomial model with linear, interactive and quadratic terms is selected to explain the effects of process variables on CO<sub>2</sub> Capture [16]. Final second order polynomial model obtained in terms of coded factors are given below.

$$\text{CO}_2 \text{ Capture (mg/g of adsorbent)} = 958 - 36.25A - 4.25B + 48.50C + 179AB - 91.50AC - 59.50BC - 250.50A^2 - 71.50B^2 - 96C^2 \quad (1)$$

TABLE I STATISTICAL DESIGN OF EXPERIMENTS

S. No.	A	B	C	R1
1	50	35	0.2	958
2	50	35	0.2	958
3	50	35	0.2	958
4	75	35	0.1	590
5	75	15	0.2	424
6	25	35	0.3	816
7	50	55	0.3	746
8	75	35	0.3	520
9	50	15	0.1	716
10	50	35	0.2	958
11	25	35	0.1	520
12	50	35	0.2	958
13	50	15	0.3	916
14	25	15	0.2	814
15	25	55	0.2	490
16	75	55	0.2	816
17	50	55	0.1	784

TABLE II SEQUENTIAL MODEL SUM OF SQUARE AND MODEL SUMMARY STATISTICS FOR RESPONSE

Model	Model summary statistics					
	Std.Dev.	R <sup>2</sup>	Adjusted R <sup>2</sup>	Predicted R <sup>2</sup>	Press	Remarks
<b>CO<sub>2</sub> Capture</b>						
Linear	202.4170	0.0524	-0.1662	-0.6516	928392.1	
2FI	188.8996	0.3652	-0.0157	-0.8817	1057735.5	
Quadratic	32.5247	0.9868	0.9699	0.7892	118480.0000	Suggested
Cubic	0.0000	1.0000	1.0000		+	Aliased
Source	Sum of Squares	Df	Mean Square	F Value	Prob > F	Remarks
<b>Sequential model sum of squares for CO<sub>2</sub> Capture</b>						
Mean	9852668.47	1.00	9852668.47			
Linear	29475.00	3.00	9825.00	0.24	0.8670	
2FI	175814.00	3.00	58604.67	1.64	0.2415	
Quadratic	349425.53	3.00	116475.18	110.10	< 0.0001	Suggested
Cubic	7405.00	3.00	2468.33	63660000.00	< 0.0001	Aliased

Where, A, B and C are temperature, feed flow rate and mass of the adsorbent, respectively. In order to validate the capability of developed second order polynomial model, experimental values are selected randomly from selected process variable ranges and are plotted with model predicted versus actual plots. The data points on this plot lie very close to the diagonal line indicates (Fig. 4) the good

adequate agreement between experimental data. Moreover, P (<0.0001) and F (>1) values of response indicates the suitability of developed mathematical models. From these results (Table III), it is concluded that the developed mathematical models can describe the extraction process very robustly.

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CO<sub>2</sub> Capture (mg/ g of adsorbent):

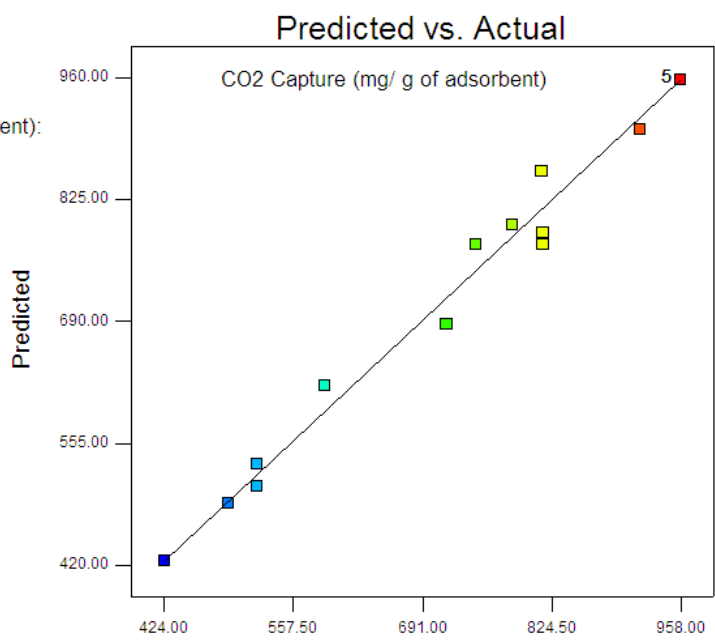


Fig. 4 Perturbation plot for CO<sub>2</sub> capture

TABLE IV ANOVA RESULTS FOR CO<sub>2</sub> CAPTURE

Source	Sum of Squares	df	Mean Square	F Value	p-value Prob > F	Remarks
Model	554715	9	61634.9	58.264	< 0.0001	significant
A-Temperature (°C)	10512.5	1	10512.5	9.93754	0.0161	
B-Flow rate (ml/min)	144.5	1	144.5	0.1366	0.7226	
C-Mass of adsorbent (g)	18818	1	18818	17.7888	0.0039	
AB	128164	1	128164	121.154	< 0.0001	
AC	33489	1	33489	31.6574	0.0008	
BC	14161	1	14161	13.3865	0.0081	
A2	264212	1	264212	249.761	< 0.0001	
B2	21525.3	1	21525.3	20.348	0.0028	
C2	38804.2	1	38804.2	36.6819	0.0005	
Residual	7405	7	1057.86			
Lack of Fit	7405	3	2468.33			
Pure Error	0	4	0			
Cor Total	562120	16				

E. Optimization and Validation

In order to determine the optimum operating conditions for CO<sub>2</sub> capture in packed bed column, numerical optimization technique is applied. Optimal operating conditions to obtain the maximum electricity from MFC are found to be as follows: temperature of 40°C, feed flow rate of 30 ml/min and 0.25 g of the Poly-(D) glucosamine. Under these optimal conditions, predicted CO<sub>2</sub> capture is found to be 956 mg CO<sub>2</sub> with desirability value of 0.9854. The confirmation experiment is carried out in aforementioned conditions and the result obtained is close agreement with predicted one [17-18].

IV. CONCLUSION

This study focused on CO<sub>2</sub> capture in packed bed column reactor using Poly-(D) glucosamine under the various process parameters such as temperature, feed flow rate and mass of the adsorbent. Individual and interactive effective of process parameters on the CO<sub>2</sub> capture is examined statistically. The developed second order polynomial model is examined ANOVA and actual versus predicted plot. Numerical optimization is used to optimize the process parameters to capture maximum CO<sub>2</sub>. The maximum of 956 mg CO<sub>2</sub> is captured under the following operating conditions; temperature of 40°C, feed flow rate of 30

ml/min and 0.25 g of the Poly-(D) glucosamine. Also, under various conditions experiments were performed in order to verify the reliability of statistical analyses and results were confirmed. Hence, CO<sub>2</sub> capture in packed bed column reactor using Poly-(D) glucosamine is a promising method which will help to solve the global warming and climate change issues.

## REFERENCES

- [1] A. L. Anwar, G. N. Halder and A. K. Sahab, "Experimental investigation on efficient carbon dioxide capture using piperazine (PZ) activated aqueous methyldiethanolamine (MDEA) solution in a packed column", *International Journal of Greenhouse Gas Control*, Vol. 64, pp. 163-173, 2017.
- [2] C. Chen, J. Kim, D. Park and W. Ahn, "Ethylendiamine grafting on zeolite like metal organic frameworks (ZMOF) for CO<sub>2</sub> capture", *Materials letters*, Vol. 78, pp. 344-347, 2013.
- [3] C. Chen, J. Kim, D. Yang, and W. Ahn, "Carbon dioxide adsorption over zeolite-like metal organic frameworks (ZMOFs) having a sodtopology: structure and ion exchange effect", *Chemical Engineering Journal*, Vol. 168, pp. 1134-1139, 2011.
- [4] T. Chitsiga, M. Daramola, N. Wagner and J. Ngoy, "Effect of the presence of water-soluble amines on the carbon dioxide (CO<sub>2</sub>) adsorption capacity of amine-grafted polysuccinimide (PSI) adsorbent during CO<sub>2</sub> capture", *Energy Procedia*, Vol. 90, pp. 105-86, 2016.
- [5] W. Haohan, G. Charles, S. Thibault, W. Hao and A. Katie, "Effect of temperature on hydrogen and carbon dioxide adsorption hysteresis in an ultramicroporous MOF", *Microporous and Mesoporous Materials*, Vol. 5, pp. 186-189, 2016.
- [6] A. Imteaz and H. Sung, "Composite of metal organic framework: Preparation and Application in adsorption", *Materials today*, Vol. 24, pp. 138-146, 2014.
- [7] J. Lin, D. Kang, H. Shan, S. Shi and T. Chung, "A comparison between packed beds and rotating packed beds for CO<sub>2</sub> capture using monoethanolamine and dilute aqueous ammonia solutions", *International Journal of Greenhouse Gas Control*, Vol. 46, pp. 228-239, 2016.
- [8] W. Lei, J. Wang, Z. Zhang, T. Ziting, S. Jiang and L. Chunrong, "Development of Ionic Liquids Tethered to Coconut Shell Activated Carbon for Biogas Upgrading in a Packed Bed", *Energy Technol.*, Vol. 3, pp. 509-517, 2015.
- [9] J. Ma, C. Xin and C. Tan, "Preparation, physicochemical and pharmaceutical characterization of chitosan from *Catharsius molossus* residue", *International Journal of Biological Macromolecules*, Vol. 15, pp. 547-556, 2015.
- [10] W. Ningning, Z. Yan, C. Changhong, C. Linyu and D. Hanming, "A g-C<sub>3</sub>N<sub>4</sub> supported graphene oxide/Ag<sub>3</sub>PO<sub>4</sub> composite with remarkably enhanced photocatalytic activity under visible light", *Catalysis Communications*, Vol. 15, pp. 68-73, 2015.
- [11] J. Prakash Maran, V. Sivakumar, R. Sridhar and K. Thiruganasambandham, "Artificial neural network and response surface methodology modeling in mass transfer parameters predictions during osmotic dehydration of Carica papaya L", *Alexandria Engineering Journal*, Vol. 52, pp. 507-516, 2013.
- [12] S. Praveen and P. P. Selvi, "Absorption of Carbon dioxide in Packed Column", *International Journal of Scientific and Research Publications*, Vol. 4, pp. 1-11, 2014.
- [13] J. Rowsell and O. Yaghi, Metal-organic frameworks: a new class of porous materials, *Microporous and Mesoporous Materials*, Vol. 3, pp. 14-22, 2004.
- [14] G. Shaohua, L. Pan, Y. Haijun, Z. Yanbei, C. Mingwei, I. Masayoshi, and Z. Haoshen, "A Layered P<sub>2</sub>- and O<sub>3</sub>-Type Composite as a High-Energy Cathode for Rechargeable Sodium-Ion Batteries", *Ind. Eng. Chem. Res.*, Vol. 54, pp. 5894 - 5900, 2015.
- [15] K. Thiruganasambandham and V. Sivakumar, "Eco-friendly approach of copper (II) ion adsorption on to cotton seed cake and its characterization: Simulation and Validation", *Journal of the Taiwan Institute of Chemical Engineers*, Vol. 50, pp. 198-204, 2015.
- [16] M. Wang, A. Lawal, P. Stephenson, J. Sidders and C. Ramshaw, "Post-combustion CO<sub>2</sub> capture with chemical absorption: A state-of-the-art review", *Chemical Engineering Research and Design*, Vol. 11, pp. 1609-1624, 2011.
- [17] C. Yu, C. Huang and C. Tan, "A Review of CO<sub>2</sub> Capture by Absorption and Adsorption", *Taiwan Association for Aerosol Research*, Vol. 12, pp. 745-769, 2012.
- [18] Q. Yu, D. W. F. Brilman, "Design Strategy for CO<sub>2</sub> Adsorption from Ambient Air Using a Supported Amine Based Sorbent in a Fixed Bed Reactor", *Energy Procedia*, Vol. 11, pp. 6102-6114, 2017.